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# Sorption equilibrium of mercury onto ground-up tree fern

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### **Abstract**

The sorption behavior of mercury at different temperatures onto ground-up tree fern was investigated. The experimental results were fitted to two two-parameter isotherms, the Freundlich and Langmuir isotherms, as well as to two three-parameter isotherms, the Redlich–Peterson and Sips isotherms to obtain the characteristic parameters of each model. A comparison of best-fitting was performed using the coefficient of determination and Chi-square test. Both the Langmuir and Redlich–Peterson isotherms were found to well represent the measured sorption data. According to the evaluation using the Langmuir equation, the saturated monolayer sorption capacity of mercury ions onto ground-up tree fern was 26.5 mg/g at 298 K. It was noted that an increase in temperature resulted in a higher mercury ion loading per unit weight of the tree fern. In addition, various thermodynamic parameters, such as  $\Delta G^{\circ}$ ,  $\Delta H^{\circ}$ , and  $\Delta S^{\circ}$ , were calculated and compared with the sorption of mercury by other sorbents. © 2008 Elsevier B.V. All rights reserved.

Keywords: Agriculture product; Adsorption; Mercury; Tree fern; Biosorption

## 1. Introduction

Understanding the sorption of metal ions from aqueous solutions is important in water pollution control. The application of low-cost sorbents including carbonaceous materials, agricultural products, and waste by-products has been investigated. In recent years, agricultural waste materials and by-products of cellulosic origin have been widely studied in the literature for their capacity to remove mercury from aqueous solutions. These include peat [1], bark [2], cellulose [3], lignite [4], coconut husks [5], rice husks [6], Sugi wood [7], flax shive [8], bagasse pith [9], moss [10], vegetables [11], carbonised coirpith [12], rice-husk ash [13], tea leaves, and coffee beans [14]. Several extensive studies have also been performed using activated carbon prepared from agricultural wastes for the removal of mercury from aqueous solutions such as peanut hull carbon [15], olive stones [16], and Sugi wood [17]. In addition, chemically treated sorbents including coconut husks [18], bagasse pith [19], bark [20], and polyacrylamide-grafted banana stalks [21], have been used in attempts to enhance the mercury sorption performance. Most of this work has shown that agricultural products and waste byproducts can be good sorbents for heavy metals. Many of these natural sorbents remove metals more by ion exchange than by adsorption.

The structure of tree fern is cellulose based [22], and the surface of the cellulose in contact with water is negatively charged [23]. All chemical sorbents have polar functional groups (alcohols, aldehydes, ketones, acids, phenolic hydroxides, and ethers) for chemical binding [24]. The tree fern is highly polar and has been used as a specific sorbent to remove metals such as lead [25], copper [26], cadmium [27,28], and zinc [29], as well as dye [30]. In addition, the sorption of sodium ions by tree fern showed a lower sorption capacity [23]. However, arsenical anions cannot be removed from solution because of the negative charge of the surface of tree fern material.

Several sorption isotherms have recently been studied for metal removal such as Langmuir [31], Freundlich [32], Dubinin–Radushkevich [5], Frumkin [33], van Bemmelen–Freundlich [34], Sips [35], Ideal Adsorption Solution Theory [36], BET [37], Redlich–Peterson [29], Henry [38], and Tóth [39]. The goal of the present work was to study the possibility of utilizing ground-up tree fern for the sorption of mercury ions from aqueous solutions and the effect of temperature on its sorption of mercury. In this study, Chi-square test was used, and the isotherm parameters were determined using the method of least squares. Two two-parameter isotherms, the

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Freundlich and Langmuir isotherms, as well as two three-parameter isotherms, the Redlich–Peterson and Sips isotherms, were examined for their ability to model the equilibrium sorption data. A comparison of linear and non-linear correlation analyses of these four isotherms was applied by using the sorption of mercury by ground-up tree fern.

## 2. Materials and methods

## 2.1. Materials

Raw tree fern material was dried in an oven at  $100\,^{\circ}\text{C}$  for a period of 24 h, and then ground-up and screened through a set of sieves to obtain a geometrical size of  $61\text{--}74\,\mu\text{m}$ . This produced uniform material for the complete set of sorption tests; this material was stored in an air-tight plastic container for use in all investigations. Analytical grade reagents were used in all cases. Stock solutions of mercury(II) ( $1000\,\text{mg/dm}^3$ ) were prepared in distilled water using mercury HgCl<sub>2</sub>. All working solutions were prepared by diluting the stock solution with distilled water.

# 2.2. Methods

Batch sorption experiments were performed at the desired temperatures (10, 15, 20, and 25 °C) on a rotary shaker at 100 rpm using 125-ml capped conical flasks. In each set of experiments, a range of initial metal ion concentrations was used of from 55 to 145 mg/dm<sup>3</sup>, and 0.25 g of ground-up tree fern was thoroughly mixed into 50 ml of the mercury solution. After shaking the flasks for 12 h, the tree fern material was separated by centrifugation, and the remaining mercury concentration of the solution was analyzed using inductively coupled plasma atomic emission spectroscopy (ICP-AES).

## 3. Equilibrium isotherms

Sorption equilibria provide fundamental physicochemical data for evaluating the applicability of sorption processes as a unit operation. The sorption equilibrium is usually described by an isotherm whose parameters express the surface properties and affinity of the sorbent at a fixed temperature. In order to investigate the sorption isotherms, four equilibrium models frequently applied to the sorption of metals from aqueous solution were fitted to the experimental results. These included two two-parameter isotherms, the Langmuir and the Freundlich isotherms, as well as two three-parameter isotherms, the Redlich–Peterson and the Sips isotherms.

The equilibrium sorption capacity is obtained by using a mass balance equation:

$$q_{\rm e} = \frac{(C_0 - C_{\rm e})V}{m_{\rm s}};$$
 (1)

where  $C_0$  and  $C_e$  are the initial and equilibrium concentration, respectively (mg/dm<sup>3</sup>), V is the volume of solution used (dm<sup>3</sup>), and  $m_s$  is the sorbent mass (g).

## 3.1. Langmuir isotherm

The saturated monolayer Langmuir isotherm [40] can be represented as:

$$q_{\rm e} = \frac{q_{\rm m} K_{\rm a} C_{\rm e}}{1 + K_{\rm a} C_{\rm e}}.\tag{2}$$

The constants  $q_{\rm m}$  and  $K_{\rm a}$  are the characteristic of the Langmuir equation and can be determined from a linearised form of Eq. (2), represented by

$$\frac{C_{\rm e}}{q_{\rm e}} = \frac{1}{q_{\rm m}K_{\rm a}} + \frac{C_{\rm e}}{q_{\rm m}}.\tag{3}$$

A plot of  $C_e/q_e$  versus  $C_e$  should indicate a straight line of slope  $1/q_m$  and an intercept of  $1/(K_a q_m)$ , or alternatively

$$\frac{1}{q_{\rm e}} = \left(\frac{1}{K_{\rm a}q_{\rm m}}\right) \times \frac{1}{C_{\rm e}} + \frac{1}{q_{\rm m}} \tag{4}$$

which is a straight line with a slope of  $1/(K_a q_m)$  and an intercept of  $1/q_m$  when plotting  $1/q_e$  versus  $1/C_e$ ; where  $C_e$  is the equilibrium concentration (mg/dm<sup>3</sup>),  $q_e$  is the amount of mercury sorbed (mg/g),  $q_m$  is  $q_e$  for a complete monolayer (mg/g), and  $K_a$  is the sorption equilibrium constant (dm<sup>3</sup>/mg) [29].

#### 3.2. Freundlich isotherm

The Freundlich isotherm [41] is expressed by the following equation:

$$q_{\rm e} = K_{\rm F} C_{\rm e}^{1/n}. \tag{5}$$

The equation may be linearised by taking the logarithm of both sides

$$\log(q_{\rm e}) = \frac{1}{n}\log(C_{\rm e}) + \log(K_{\rm F}) \tag{6}$$

which produces a straight line with a slope of 1/n and an intercept of  $\log{(K_{\rm F})}$  when plotting  $\log{(q_{\rm e})}$  versus  $\log{(C_{\rm e})}$ .

# 3.3. Redlich-Peterson isotherm

The Redlich–Peterson isotherm [42] contains three parameters and involves features of both the Langmuir and the Freundlich isotherms. It can be described as follows:

$$q_{\rm e} = \frac{AC_{\rm e}}{1 + BC_{\rm e}^g}.\tag{7}$$

Taking the natural logarithm of both sides results in

$$\ln\left(A\frac{C_{\rm e}}{q_{\rm e}} - 1\right) = g\ln(C_{\rm e}) + \ln(B). \tag{8}$$

Although, a linear analysis is not possible for a threeparameter isotherm, three isotherm constants, A, B, and g, can be evaluated from the pseudo-linear plot represented by Eq. (8) using a trial and error optimization method. A general trial and error procedure which is applicable to computer operations was developed to determine the coefficient of determination,  $r^2$ , for a series of values of A for the linear regression of  $\ln(C_e)$  on  $\ln [A(C_e/q_e) - 1]$  and to obtain the best value of A which yields a maximum 'optimized' value of  $r^2$ .

# 3.4. Sips isotherm

The Sips [43] or Langmuir–Freundlich isotherm also contains three parameters. The isotherm can be represented as

$$q_{\rm e} = \frac{A_{\rm S} C_{\rm e}^{C_{\rm S}}}{1 + A_{\rm S} C_{\rm e}^{C_{\rm S}}};\tag{9}$$

or, in the Langmuir-Freundlich form:

$$q_{\rm e} = \frac{q_{\rm m} K_{\rm a} C_{\rm e}^{K_{\rm LF}}}{1 + K_{\rm a} C_{\rm e}^{K_{\rm LF}}}.$$
 (10)

The equation may be linearised by taking the natural logarithm of both sides:

$$\ln\left(\frac{q_{\rm e}}{q_{\rm m} - q_{\rm e}}\right) = K_{\rm LF} \ln(C_{\rm e}) + \ln(K_{\rm a}). \tag{11}$$

Three isotherm constants,  $q_{\rm m}$ ,  $K_{\rm LF}$ , and  $K_{\rm a}$ , can be evaluated from the pseudo-linear plot represented by Eq. (11) using a trial and error optimization method. A general trial and error procedure which is applicable to computer operations was developed to determine the coefficient of determination,  $r^2$ , for a series of values of  $q_{\rm m}$  for the linear regression of  $\ln{(C_{\rm e})}$  on  $\ln{[q_{\rm e}/(q_{\rm m}-q_{\rm e})]}$  and to obtain the best value of  $q_{\rm m}$  which yields a maximum 'optimized' value of  $r^2$ .

# 3.5. Error analysis

In the single-component isotherm studies, the optimization procedure requires an error function to be defined in order to be able to evaluate the fit of the isotherm to the experimental equilibrium data. In this study, linear coefficients of determination and non-linear Chi-square test were examined.

The Chi-square test statistic is basically the sum of the squares of the differences between the experimental data and data obtained by calculating using the models, with each squared difference divided by the corresponding data obtained by calculating using the models. The equivalent mathematical statement is

$$\chi^2 = \sum \frac{(q_e - q_{e,m})^2}{q_{e,m}};$$
 (12)

where  $q_{e,m}$  is the equilibrium capacity obtained by calculating using the model (mg/g) and  $q_e$  is the experimental data of the equilibrium capacity (mg/g). If data from a model are similar to the experimental data,  $\chi^2$  will be a small number, and if they are different,  $\chi^2$  will be a big number. Therefore, it is necessary to also analyze the data set of the Chi-square test to confirm the best-fit isotherm for the sorption system.

# 4. Results and discussion

The simplest method to determine isotherm constants for twoparameter isotherms is to transform the isotherm variables so that the equation is converted to a linear form and then to apply a

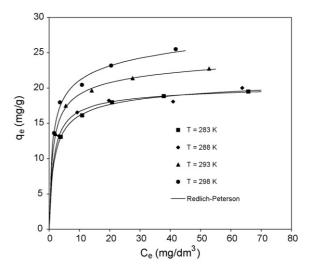


Fig. 1. Redlich-Peterson isotherms for the sorption of mercury ions using ground-up tree fern at various temperatures.

linear regression. Least square is the most common method for fitting a straight line through experimental results. The principle behind least squares is to find the line that optimizes the coefficient of determination,  $r^2$ , or correlation coefficient, r, between the experimental points and the straight line.

Sorption isotherms of mercury ions onto ground-up tree fern at various solution temperatures are shown in Fig. 1. The Langmuir ( $K_a$  and  $q_m$ ) and Freundlich ( $K_F$  and 1/n) constants were calculated from the plots of  $C_e/q_e$  versus  $C_e$  and  $\log q_e$  versus  $\log C_e$ , respectively, using a linear least squares fitting (Table 1). For the three-parameter isotherm, Redlich–Peterson and Langmuir–Freundlich constants were also obtained by a trial and error method using the plots of  $\ln(C_e)$  versus  $\ln[A(C_e/q_e)-1]$  and  $\ln(C_e)$  versus  $\ln[q_e/(q_m-q_e)]$ , from the linear isotherm forms of Eqs. (8) and (11), respectively. Fig. 2 shows the different isotherms for sorption of mercury onto ground-up tree fern. Comparison of the linear regression coefficient of determination,  $r^2$ , and the non-linear Chi-square analysis,  $\chi^2$  which were calculated by Eq. (12), are shown in

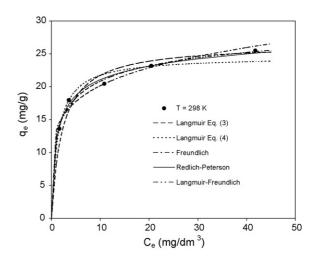
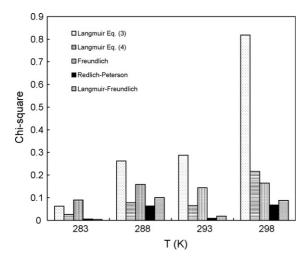


Fig. 2. Comparison of different isotherms for the sorption of mercury by ground-up tree fern.

Table 1	
Constants for Langmuir Eq. (3), Langmuir Eq. (4), Freundlich, Redlich–Peterson, and Langmuir–Freundlich isotherms	

T(K)	Langmuir Eq. (3)		Langmuir Eq. (4)		Freundlich		Redlich-Peterson		Langmuir-Freundlich				
	$q_{ m m}$	Ka	$q_{ m m}$	Ka	$\Delta G^{\circ}$	$K_{\mathrm{F}}$	1/n	g	A	В	$K_{ m LF}$	Ka	$q_{ m m}$
283	20.2	0.401	19.7	0.502	-10.9	11.2	0.142	0.950	13.6	0.837	0.738	0.601	21.0
288	20.3	0.423	19.6	0.628	-11.6	11.9	0.127	0.973	14.6	0.826	0.371	0.753	25.4
293 298	23.5 26.5	0.471 0.454	22.4 24.6	0.687 0.762	-12.0 $-12.5$	12.6 13.2	0.158 0.183	0.943 0.916	21.1 28.9	1.15 1.54	0.573 0.462	0.721 0.594	25.9 32.9



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Fig. 3. Comparison of non-linear Chi-square test analysis,  $\chi^2$ .

Figs. 3 and 4. The results indicate that the three-parameter Redlich–Peterson isotherm exhibits the best-fit with the highest value of  $r^2$  and lowest value of  $\chi^2$ . Both three-parameter isotherms of Redlich–Peterson and Langmuir–Freundlich have lower values of  $\chi^2$  than these of the two-parameter isotherms. Even though the most suitable isotherm for the data set was the Redlich–Peterson isotherm, the difference between the two linear forms of the Langmuir isotherm significantly affected the result. Values of  $r^2$  obtained from the linear Langmuir Eq. (3)

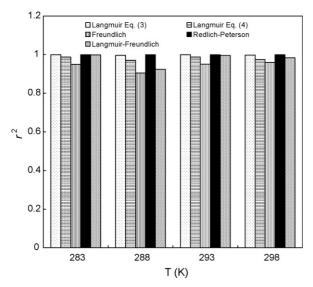


Fig. 4. Comparison of linear regression coefficients of determination,  $r^2$ .

were consistently higher than these of Langmuir Eq. (4). However, the value of  $\chi^2$  shows that the Langmuir Eq. (4) produced a better fit than Eq. (3). This denotes that a different axis setting would alter the results of a linear regression and hence influence the determination process. Unlike the linear analysis, different forms of the equations would significantly effect  $r^2$  and impact the final determination, whereas the non-linear Chi-square analysis is a method which avoids such errors [44].

Values of  $\chi^2$  were compared to determine the appropriate type of two-parameter isotherm for mercury sorption.  $\chi^2$  values for the fitting of mercury to the theoretical Langmuir Eq. (4) isotherm were lower than the values for the empirical Freundlich isotherm, as shown in Fig. 3. Hence, the Langmuir isotherm agrees well with the experimental data, assuming that all of the sorption sites have equal energy [40].

The effect of the isotherm shape can be used to predict the favorableness or unfavorableness of a sorption system in batch processes.

The effect of the isotherm shape can be used to predict if a sorption system is 'favorable' or 'unfavorable' in batch processes [45]. According to Hall et al. [46], the essential features of the Langmuir isotherm can be expressed in terms of a dimensionless constant separation factor or equilibrium parameter,  $K_R$ , which is defined by the following relationship:

$$K_{\rm R} = \frac{1}{1 + K_2 C_0};\tag{13}$$

where  $K_R$  is a dimensionless separation factor,  $C_0$  is the initial concentration (mg/dm<sup>3</sup>), and  $K_a$  is the Langmuir constant (dm<sup>3</sup>/mg). The parameter  $K_R$  indicates the shape of the isotherm according the following table

Values of $K_R$	Type of isotherm
$K_{\rm R} > 1$	Unfavorable
$K_{\rm R} = 1$	Linear
$0 < K_{\rm R} < 1$	Favorable
$K_{\rm R} = 0$	Irreversible

The relationship between the parameter  $K_R$  and  $C_0$  was reported as a figure [29]. The values of  $K_R$  for mercury are given in Fig. 5. The  $K_R$  values indicate that sorption is more favorable for the higher initial mercury concentrations than for lower ones. Referring to Fig. 5, it is obvious that ground-up tree fern is a good sorbent for mercury. The sorption is more favorable at higher temperatures.

The monolayer coverage,  $q_{\rm m}$ , obtained from the Langmuir isotherm for each temperature increased with increasing temper-

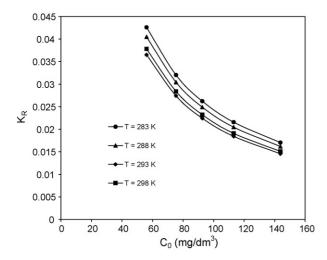


Fig. 5. Plot of  $K_R$  against initial mercury ion concentration at various temperatures.

ature (Table 1). Increasing the temperature is known to increase the rate at which chemisorption and diffusion processes occur. Typical chemisorption involving valence forces through the sharing or exchange of electrons between the sorbent and sorbate, is an endothermic process, thus chemisorption may play a significant role in the sorption process. In addition, increasing the temperature may produce a swelling effect within the internal structure of the tree fern material enabling metal ions to penetrate further [47] or to the creation of some new active sites on the sorbent surface [6].

The plateau on each isotherm corresponds to monolayer coverage of the surface by the metal ions, and this value is the ultimate sorptive capacity at high concentrations which can be used to estimate the specific surface area, S, of ground-up tree fern using the following equation:

$$S = \frac{q_{\rm m}NA}{M};\tag{14}$$

where S is the specific surface area in m<sup>2</sup>/g tree fern,  $q_{\rm m}$  is the monolayer sorption capacity in g metal/g tree fern, N is Avogadros number (6.02 × 10<sup>23</sup>), A is the cross-sectional area of metal ion in m<sup>2</sup>, and M is the molecular weight of the metal. A comparison of the specific surface area for sorption of divalent metal ions was made by using the monolayer sorption capacity,  $q_{\rm m}$ , which was obtained from previous work [28,29]. Therefore, the specific surface areas can be calculated by Eq. (14) for Zn<sup>2+</sup>, Cu<sup>2+</sup>, Pb<sup>2+</sup>, Cd<sup>2+</sup>, and Hg<sup>2+</sup> (Table 2). The specific surface area of ground-up tree fern for the metal ions was affected by the

Table 2 Specific surface areas and saturated monolayer capacities for metals by ground-up tree fern

Metal	Ionic radius (Å)	M	$A (m^2)$	$q_{\rm m}$ (mg/g)	$S (m^2/g)$
Zn <sup>2+</sup>	0.88	65.38	$2.43 \times 10^{-20}$	7.58	1.70
Cu <sup>2+</sup>	0.87	63.546	$2.38 \times 10^{-20}$	10.6	2.39
$Cd^{2+}$	1.09	112.41	$3.73 \times 10^{-20}$	16.3	3.26
Hg <sup>2+</sup>	1.16	200.59	$4.23 \times 10^{-20}$	26.5	3.36
Pb <sup>2+</sup>	1.33	207.2	$5.56 \times 10^{-20}$	39.8	6.43

divalent metal characteristics such as ionic radius and molecular weight. In general, the area increased with an increase in the monolayer sorption capacity and the specific surface areas except for zinc which had a lower monolayer sorption capacity and specific surface areas compared copper. The same sorption capacity order ( $Cu^{2+} > Zn^{2+}$ ) occurred in the sorption of metals by natural zeolite [48], low-rank Turkish coals [49], and native sugar beet pulp [50]. The specific surface area of ground-up tree fern was in the order of  $Zn^{2+} < Cu^{2+} < Cd^{2+} < Hg^{2+} < Pb^{2+}$ .

In environmental engineering practice, both energy and entropy factors must be considered in order to determine what processes will occur spontaneously. Gibb's free energy change,  $\Delta G^{\circ}$ , is the fundamental criterion of spontaneity. Reactions occur spontaneously at a given temperature if  $\Delta G^{\circ}$  is a negative value. The thermodynamic parameters of Gibb's free energy change,  $\Delta G^{\circ}$ , enthalpy change,  $\Delta H^{\circ}$ , and entropy change,  $\Delta S^{\circ}$ , for the sorption processes are calculated using the following equations:

$$\Delta G^{\circ} = -RT \ln K_{\rm a} \tag{15}$$

and

$$\Delta G^{\circ} = \Delta H^{\circ} - T \Delta S^{\circ}, \tag{16}$$

where R is universal gas constant (8.314 J/mol K) and T is the absolute temperature in K.

The thermodynamic parameters Gibb's free energy change,  $\Delta G^{\circ}$ , are calculated using  $K_{\rm a}$  which is obtained from Langmuir Eq. (4) and are shown in Table 1. A plot of Gibb's free energy change,  $\Delta G^{\circ}$ , versus temperature, T, was found to be linear (Fig. 6). The enthalpy change,  $\Delta H^{\circ}$ , and the entropy change,  $\Delta S^{\circ}$ , for the sorption processes were obtained from the intercept and slope of Eq. (16) and found to be 18.8 kJ/mol and 0.105 kJ/mol K, respectively. The negative values of  $\Delta G^{\circ}$  confirm the feasibility of the process and the spontaneous nature of sorption with a high preference of mercury ions by ground-up tree fern. The decrease in the negative value of  $\Delta G^{\circ}$  with an increase in temperature indicates that the sorption process of mercury ions on ground-up tree fern becomes more favorable at higher temperatures [51]. In most cases, sorption of mer-

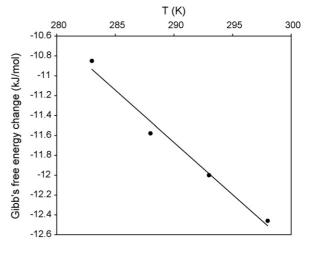


Fig. 6. Plot of Gibb's free energy change,  $\Delta G^{\circ}$ , versus temperature, T.

Table 3

A comparison of thermodynamic parameters for the sorption of mercury by different sorbents

Sorbent	$\Delta G^{\circ}$ (kJ/mol)	$\Delta H^{\circ}$ (kJ/mol)	ΔS° (kJ/mol K)	References
Polyurethane (PUR)	Negative	-30.7	-70.1	[56]
Activated carbon	Negative	-23.6	-20.5	[55]
Sawdust	Negative	20.9	87.4	[54]
Polyacrylamide-grafted iron(III) oxide	Negative	26.3	100	[53]
Polyacrylamide-grafted banana stalk	Negative	32.1	169	[21]
2-Mercaptobenzimidazole- clay	Negative	34.8	190	[52]
Demineralized lignite coal	Negative	-2.6	0.024	[4]

cury was found to have negative values of  $\Delta G^{\circ}$  (Table 3). The value of  $\Delta H^{\circ}$  is positive, indicating that the sorption reaction is endothermic. However, not all the mercury sorption systems were endothermic (Table 3). Entropy has been defined as the degree of chaos of a system. A positive value of  $\Delta S^{\circ}$  reflects increasing randomness at the solid/liquid interface during the sorption of mercury ions on the sorbent [6,21,52]. There are consistencies in the sorption of mercury by other sorbents, for example, rice husks [6], polyacrylamide-grafted iron(III) oxide [53], 2-mercaptobenzimidazole-clay [52], sawdust [54], demineralized lignite coal [4], and polyacrylamide-grafted banana stalks [21]. However, a negative value for  $\Delta S^{\circ}$  was also reported for the sorption of mercury by activated carbon derived from fertilizer waste [55] and for the sorption of Hg(II)-SCN on polyurethane foam [56]. In addition, there are two conclusions for the sorption of mercury presented in the literature. The first is that a relatively small positive value of  $\Delta S^{\circ}$  indicates that no significant structural change occurs in the sorbent [21,53]. The other is that the positive value of  $\Delta S^{\circ}$  reflects the affinity of the ground-up tree fern for mercury ions and suggests some structural changes in both the mercury and sorbent [52].

# 5. Conclusion

Ground-up tree fern is able to sorb mercury ions from aqueous solutions. The mercury ion binding capacity of ground-up tree fern was a function of temperature. The sorption capacity increased with increasing temperature. It is not appropriate to use the coefficient of determination of the linear regression analysis for comparing the best-fit of the Redlich-Peterson, Sips, Freundlich, and both linear Langmuir isotherms. The results from this study were extremely well described by the threeparameter Redlich-Peterson isotherm. The negative values of  $\Delta G^{\circ}$  indicate the spontaneous nature of sorption with a high preference of mercury ions on ground-up tree fern, and that the sorption reaction is endothermic in which there is increasing randomness at the solid/liquid interface during the sorption of mercury ions onto ground-up tree fern. The monolayer sorption capacity and the specific surface areas of tree fern for divalent metal ions were affected by the metal ionic radius and molecular weight.

## References

- M. Lodenius, A. Seppanen, A. Uusirauva, Sorption and mobilization of mercury in peat soil, Chemosphere 12 (1983) 1575–1581.
- [2] G. Vázquez, J. González-Álvarez, S. Freire, M. López-Lorenzo, G. Antorrena, Removal of cadmium and mercury ions from aqueous solution by sorption on treated *Pinus pinaster* bark: kinetics and isotherms, Bioresour. Technol. 82 (2002) 247–251.
- [3] R.R. Navarro, K. Sumi, N. Fujii, M. Matsumura, Mercury removal from wastewater using porous cellulose carrier modified with polyethyleneimine, Water Res. 30 (1996) 2488–2494.
- [4] C.A. Eligwe, N.B. Okolue, C.O. Nwambu, C.I.A. Nwoko, Adsorption thermodynamics and kinetics of mercury(II), cadmium(II) and lead(II) on lignite, Chem. Eng. Technol. 22 (1999) 45–49.
- [5] S.M. Hasany, R. Ahmad, M.H. Chaudhary, Investigation of sorption of Hg(II) ions onto coconut husk from aqueous solution using radiotracer technique, Radiochim. Acta 91 (2003) 533–538.
- [6] N. Khalid, S. Ahmad, S.N. Kiani, J. Ahmed, Removal of mercury from aqueous solutions by adsorption to rice husks, Sep. Sci. Technol. 34 (1999) 3139–3153.
- [7] L.L. Pulido, T. Hata, Y. Imamura, S. Ishihara, T. Kajimoto, Removal of mercury and other metals by carbonized wood powder from aqueous solutions of their salts, J. Wood Sci. 44 (1998) 237–243.
- [8] M. Cox, E.I. El-Shafey, A.A. Pichugin, Q. Appleton, Removal of mercury(II) from aqueous solution on a carbonaceous sorbent prepared from flax shive, J. Chem. Technol. Biotechnol. 75 (2000) 427–435.
- [9] K.A. Krishnan, T.S. Anirudhan, Removal of mercury(II) from aqueous solutions and chlor-alkali industry effluent by steam activated and sulphurised activated carbons prepared from bagasse pith: kinetics and equilibrium studies, J. Hazard. Mater. 92 (2002) 161–183.
- [10] M. Kondoh, M. Fukuda, M. Azuma, H. Ooshima, J. Kato, Removal of mercury ion by the moss Pohlia flexuosa, J. Ferment. Bioeng. 86 (1998) 197–201.
- [11] A.V. Ponomarev, A.V. Bludenko, I.E. Makarov, A.K. Pikaev, D.K. Kim, Y. Kim, B. Han, Combined electron-beam and adsorption purification of water from mercury and chromium using materials of vegetable origin as sorbents, Radiat. Phys. Chem. 49 (1997) 473–476.
- [12] C. Namasivayam, K. Kadirvelu, Carbonised coirpith as an adsorbent for the removal of toxic ions, dyes and pesticides from wastewaters, Indian J. Chem. Technol. 5 (1998) 334–336.
- [13] D.P. Tiwari, D.K. Singh, D.N. Saksena, Hg(II) adsorption from aqueous solutions using rice-husk ash, J. Environ. Eng. -ASCE 121 (1995) 479– 481.
- [14] T. Kiyohara, K. Anazawa, H. Sakamoto, T. Tomiyasu, Adsorption of mercury on used tea leaves and coffee beans, Bunseki Kagaku 52 (2003) 887–890.
- [15] C. Namasivayam, K. Periasamy, Bicarbonate-treated peanut hull carbon for mercury(II) removal from aqueous solution, Water Res. 27 (1993) 1663–1668.
- [16] P. Galiatsatou, M. Metaxas, D. Arapoglou, V. Kasselouri-Rigopoulou, Treatment of olive mill waste water with activated carbons from agricultural by-products, Waste Manage. 22 (2002) 803–812.
- [17] L. Pulido-Novicio, Y. Kurimoto, M. Aoyama, K. Seki, S. Doi, T. Hata, S. Ishihara, Y. Imamura, Adsorption of mercury by sugi wood carbonized at 1000 °C, J. Wood Sci. 47 (2001) 159–162.
- [18] M.K. Sreedhar, T.S. Anirudhan, Preparation of an adsorbent by craft polymerization of acrylamide onto coconut husk for mercury(II) removal from aqueous solution and chloralkali industry wastewater, J. Appl. Polym. Sci. 75 (2000) 1261–1269.
- [19] K.A. Krishnan, T.S. Anirudhan, Removal of cadmium(II) from aqueous solutions by steam-activated sulphurised carbon prepared from sugarcane bagasse pith: kinetics and equilibrium studies, Water SA 29 (2003) 147–156.
- [20] I. Gaballah, G. Kilbertus, Recovery of heavy metal ions through decontamination of synthetic solutions and industrial effluents using modified barks, J. Geochem. Explor. 62 (1998) 241–286.
- [21] I.G. Shibi, T.S. Anirudhan, Synthesis, characterization, and application as a mercury(II) sorbent of banana stalk (Musa paradisiaca) Polyacrylamide

- grafted copolymer bearing carboxyl groups, Ind. Eng. Chem. Res. 41 (2002) 5341–5352.
- [22] R. Newman, Crystalline forms of cellulose in the silver tree fern *Cyathea dealbata*, Cellulose 4 (1997) 269–279.
- [23] Y.S. Ho, Removal of copper ions from aqueous solution by tree fern, Water Res. 37 (2003) 2323–2330.
- [24] E. Adler, K. Lundquist, Spectrochemical estimation of phenylcoumaran elements in lignin, Acta Chem. Scand. 17 (1963) 13–26.
- [25] Y.S. Ho, W.T. Chiu, C.S. Hsu, C.T. Huang, Sorption of lead ions from aqueous solution using tree fern as a sorbent, Hydrometallurgy 73 (2004) 55–61.
- [26] Y.S. Ho, Removal of metal ions from sodium arsenate solution using tree fern, Process Saf. Environ. Prot. 81B (2003) 352–356.
- [27] Y.S. Ho, Second-order kinetic model for the sorption of cadmium onto tree fern: a comparison of linear and non-linear methods, Water Res. 40 (2006) 119–125.
- [28] Y.S. Ho, C.C. Wang, Pseudo-isotherms for the sorption of cadmium ion onto tree fern, Process Biochem. 39 (2004) 759–763.
- [29] Y.S. Ho, C.T. Huang, H.W. Huang, Equilibrium sorption isotherm for metal ions on tree fern, Process Biochem. 37 (2002) 1421–1430.
- [30] Y.S. Ho, T.H. Chiang, Y.M. Hsueh, Removal of basic dye from aqueous solution using tree fern as a biosorbent, Process Biochem. 40 (2005) 119–124.
- [31] F. Pagnanelli, A. Esposito, L. Toro, F. Vegliò, Metal speciation and pH effect on Pb, Cu, Zn and Cd biosorption onto Sphaerotilus natans: langmuir-type empirical model, Water Res. 37 (2003) 627–633.
- [32] Z. Aksu, U. Açikel, E. Kabasakal, S. Tezer, Equilibrium modelling of individual and simultaneous biosorption of chromium(VI) and nickel(II) onto dried activated sludge, Water Res. 36 (2002) 3063–3073.
- [33] C. Quan, G. Khoe, D. Bagster, Adsorption of sodium lauryl sulfate onto arsenic-bearing ferrihydrite, Water Res. 35 (2001) 478–484.
- [34] F. Zehetner, W.W. Wenzel, Nickel and copper sorption in acid forest soils, Soil Sci. 165 (2000) 463–472.
- [35] S. Al-Asheh, F. Banat, D. Al-Rousan, Adsorption of copper, zinc and nickel ions from single and binary metal ion mixtures on to chicken feathers, Adsorpt. Sci. Technol. 20 (2002) 849–864.
- [36] F. Banat, S. Al-Asheh, F. Mohai, Multi-metal sorption by spent animal bones, Sep. Sci. Technol. 37 (2002) 311–327.
- [37] B.E. Reed, S.R. Cline, Retention and release of lead by a very fine sandy loam. I. Isotherm modelling, Sep. Sci. Technol. 29 (1994) 1529–1551.
- [38] E. Baumgarten, U. Kirchhausen-Düsing, Sorption of metal ions on alumina, J. Colloid Interface Sci. 194 (1997) 1–9.
- [39] O. Altin, H.O. Özbelge, T. Doğu, Use of general purpose adsorption isotherms for heavy metal-clay mineral interactions, J. Colloid Interface Sci. 198 (1998) 130–140.

- [40] I. Langmuir, The constitution and fundamental properties of solids and liquids, J. Am. Chem. Soc. 38 (1916) 2221–2295.
- [41] H.M.F. Freundlich, Über die adsorption in lösungen, Z. Phys. Chem. 57A (1906) 385–470.
- [42] O. Redlich, D.L. Peterson, A useful adsorption isotherm, J. Phys. Chem. 63 (1959) 1024.
- [43] R. Sips, On the structure of a catalyst surface, J. Chem. Phys. 16 (1948) 490–495.
- [44] Y.S. Ho, Selection of optimum sorption isotherm, Carbon 42 (2004) 2115–2116.
- [45] V.J.P. Poots, G. McKay, J.J. Healy, Removal of basic dye from effluent using wood as an adsorbent, J. Water Pollut. Control Fed. 50 (1978) 926–935.
- [46] K.R. Hall, L.C. Eagleton, A. Acrivos, T. Vermeulen, Pore-and solid-diffusion kinetics in fixed-bed adsorption under constant-pattern conditions, Ind. Eng. Chem. Fund. 5 (1966) 212–223.
- [47] R.K. Tiwari, S.K. Ghosh, D.C. Rupainwar, Y.C. Sharma, Managing aqueous-solutions rich in Mn(II): an inexpensive technique, Colloid Surf. A-Physicochem. Eng. Asp. 70 (1993) 131–137.
- [48] J. Perić, M. Trgo, N. Vukojević Medvidović, Removal of zinc, copper and lead by natural zeolite: a comparison of adsorption isotherms, Water Res. 38 (2004) 1893–1899.
- [49] S. Karabulut, A. Karabakan, A. Denizli, Y. Yurum, Batch removal of copper(II) and zinc(II) from aqueous solutions with low-rank Turkish coals, Sep. Purif. Technol. 18 (2000) 177–184.
- [50] Z. Reddad, C. Gérente, Y. Andres, P. Le Cloirec, Adsorption of several metal ions onto a low-cost biosorbent: kinetic and equilibrium studies, Environ. Sci. Technol. 36 (2002) 2067–2073.
- [51] A.B. Zaki, M.Y. El-Sheikh, J. Evans, S.A. El-Safty, Kinetics and mechanism of the sorption of some aromatic amines onto amberlite IRA-904 anion-exchange resin, J. Colloid Interface Sci. 221 (2000) 58–63.
- [52] D.M. Manohar, K.A. Krishnan, T.S. Anirudhan, Removal of mercury(II) from aqueous solutions and chlor-alkali industry wastewater using 2mercaptobenzimidazole-clay, Water Res. 36 (2002) 1609–1619.
- [53] G.N. Manju, K.A. Krishnan, V.P. Vinod, T.S. Anirudhan, An investigation into the sorption of heavy metals from wastewaters by polyacrylamidegrafted iron(III) oxide, J. Hazard. Mater. 91 (2002) 221–238.
- [54] S.M. Hasany, R. Ahmad, Fixation of micro or submicro amounts of Hg(II) ions onto sawdust from aqueous solutions, Main Group Met. Chem. 25 (2002) 719–726.
- [55] D. Mohan, V.K. Gupta, S.K. Srivastava, S. Chander, Kinetics of mercury adsorption from wastewater using activated carbon derived from fertilizer waste, Colloid Surf. A-Physicochem. Eng. Asp. 177 (2001) 169–181.
- [56] M.M. Saeed, S.M. Hasany, M. Ahmed, Adsorption and thermodynamic characteristics of Hg(II)-SCN complex onto polyurethane foam, Talanta 50 (1999) 625–634.